

Optimization of Aqueous Extraction Conditions for the Recovery of Phenolic Compounds and antioxidants from lemon pomace

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1 **Optimization of Aqueous Extraction Conditions for the Recovery of Phenolic**

2 **Compounds and antioxidants from lemon pomace**

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20

21 **Summary**

22 The aim of this study was to optimize the aqueous extraction conditions for the recovery of

23 phenolic compounds and antioxidant capacity of lemon pomace using response surface

24 methodology. An experiment based on Box–Behnken design was conducted to analyse the

25 effects of temperature, time and sample-to-water ratio on the extraction of total phenolic

26 compounds, total flavonoids, proanthocyanidins and antioxidant capacity. Sample-to-solvent
27 ratio had a negative effect on all the dependent variables, while extraction temperature and
28 time had a positive effect only on TPC yields and ABTS antioxidant capacity. The optimal
29 extraction conditions were 95 °C, 15 min, and a sample-to-solvent ratio of 1:100 g/ml. Under
30 these conditions, the aqueous extracts had the same content of TPC and TF as well as
31 antioxidant capacity in comparison with those of methanol extracts obtained by sonication.
32 Therefore these conditions could be applied for further extraction and isolation of phenolic
33 compounds from lemon pomace.

34

35 **Keywords** Antioxidants, phenols, flavonoids, Response Surface Methodology (RSM)

36

37 **Introduction**

38 Lemon (*Citrus limon* L.) is considered as the third most important citrus species after orange
39 and mandarin, with a strong commercial value, generating a large amount of waste. Lemon
40 peel represents the main component of waste, accounts for 50 to 65% of the whole fruit
41 weight (González-Molina *et al.*, 2010). Lemon peel contains bioactive compounds, such as
42 vitamin C (ascorbic acid), flavonoids (flavanones, flavonols, flavones) and phenolic acids
43 (ferulic, p-coumaric and sinapic acids) (Bocco *et al.*, 1998; González-Molina *et al.*, 2010),
44 which have been linked to antimicrobial (Dhanavade *et al.*, 2011), anticancer (Sun *et al.*,
45 2002) and antioxidant activities (Wilmsen *et al.*, 2005; Proteggente *et al.*, 2002).

46 Extraction of bioactive compounds and antioxidants has been achieved by both conventional
47 and non-conventional methods (Khoddami *et al.*, 2013). Several parameters affect the
48 extraction efficiency of bioactive compounds from plant tissues, including extraction time,
49 temperature, sample-to-solvent ratio, and solvent character (Sarwar *et al.*, 2012; Khoddami *et*
50 *al.*, 2013; Vuong *et al.*, 2013; Candrawinata *et al.*, 2015).

51 The solubility of bioactive compounds typically increases as a function of longer extraction
52 times and higher temperatures, resulting in higher extraction yields (Davidov-Pardo *et*
53 *al.*, 2011). However, extending extraction times and temperatures promote the degradation
54 of the bioactive compounds (Joana Gil-Chávez *et al.*, 2013; Vuong *et al.*, 2013). Several
55 solvents have been being used for the extraction of bioactive compounds from citrus;
56 methanol being the most commonly employed solvent (Abad-García *et al.*, 2007).

57 Preliminary work in our lab showed that among different solvents methanol was the most
58 efficient for the extraction of phenolic compounds and antioxidants from lemon peels
59 under ultrasound extraction (Papoutsis *et al.*, under review). Methanol is however
60 classified as a class 2 solvent, which means its use should be limited in pharmaceutical
61 products due to its inherent toxicity (FDA, 2012). Investigations to assess the effectiveness of
62 alternative, less toxic solvents to maximise the recovery of the bioactive compounds from
63 the lemon peel are therefore required. Water could be an effective solvent for the recovery
64 of phenolic compounds and antioxidants (Xu *et al.*, 2008).

65 Several studies have shown that the extraction yields of phenolic compound from plant
66 sources increase with decreasing sample-to-solvent ratio (Tan *et al.*, 2011; Dailey and Vuong,
67 2015). However, from an economical standpoint optimisation must also take
68 into consideration solvent and energy costs (Al-Farsi and Chang, 2008; Santana *et al.*, 2009).

69 Citrus waste which is a by-product generated by the citrus juice industry, contains phenolic
70 compounds which present antioxidant activities and could be validated by both
71 pharmaceutical or food industries. Organic solvents are effectively used for the extraction of
72 these compounds, however their use should be limited due to their toxicity and the risk of
73 chemical residues. Water is a safe, cheap and accessible solvent. Therefore, it is necessary to
74 optimize the extraction conditions for the maximum recovery of the bioactive compounds
75 from the lemon pomace waste, in order to minimize the production cost and obtain the safest

76 extract for further utilization. To the best of our knowledge, no studies have yet been
77 undertaken to optimise the aqueous extraction of phenolics from lemon peel. The aim of this
78 study was to use response surface methodology (RSM) to determine the optimal conditions
79 for the aqueous extraction of phenolic compounds and antioxidants from lemon peel.

80

81 **Materials and methods**

82 *Chemicals and reagents*

83 All chemicals used in this study were analytical grade. Methanol, ethanol, vanillin, and
84 potassium persulfate were purchased from Merck (Germany). Folin–Ciocalteu phenol reagent,
85 anhydrous sodium carbonate (Na_2CO_3), sodium nitrite (NaNO_2), hydrochloric acid (HCl),
86 ferric chloride (FeCl_3), gallic acid, catechin, copper (II) chloride (CuCl_2), ammonium acetate
87 (NH_4Ac), neocuproine, 2,4,6-tris(2-pyridyl)-s-triazine (TPTZ), (\pm)-6-hydroxy-2,5,7,8-
88 tetramethylchromane-2-carboxylic acid (trolox), 2,2'-azino-bis(3-ethylbenzothiazoline-6-
89 sulphonic acid) (ABTS) and 2,2-Diphenyl-1-picrylhydrazyl (DPPH) were purchased from
90 Sigma-Aldrich Co. (New South Wales, Australia). Sodium acetate trihydrate
91 ($\text{CH}_3\text{COONa}\cdot 3\text{H}_2\text{O}$) was purchased from Government Stores Department (Australia).
92 Aluminium chloride ($\text{Al}_2\text{Cl}_3\cdot 6\text{H}_2\text{O}$) was obtained from J. T. Baker Chem. Co. (Belgium).
93 Acetic acid was obtained from BDH Laboratory Supplies (Poole, England). Sodium
94 hydroxide (NaOH) was purchased from Ajax Chem. (Australia).

95

96 *Materials*

97 Lemon (*Citrus limon* L.) waste including peel and seeds (flavedo and albedo) was
98 obtained from a commercial juicing factory at Kulnura, NSW Australia. After collection,
99 the seeds were removed and the remaining peel and pomace flesh were stored immediately
100 at $-18\text{ }^\circ\text{C}$ to minimize the oxidation of the bioactive compounds. The frozen lemon waste
was immersed

101 in liquid nitrogen and freeze dried (FD3 freeze drier, Thomas Australia Pty. Ltd., Seven Hills,
102 NSW, Australia). The dried waste was ground using a commercial blender (John Morris
103 Scientific, Chatswood, NSW, Australia) and sieved using a steel mesh sieve (1.4 mm EFL
104 2000; Endecotts Ltd., London, England). The ground lemon waste was kept in a sealed
105 container at -18 °C for further analysis.

106

107 *Water Extraction process*

108 Hot water extraction of bioactive compounds was carried out by using water bath (Ratek
109 Instruments Pty. Ltd., Victoria, Australia). Specifically, a required amount of lemon dry
110 powder was mixed with distilled water according to the experimental design shown in Table
111 1. During the extraction the test tubes were wrapped with parafilm to minimize the
112 evaporation. After extraction was completed, the extracts were maintained in ice, and then
113 centrifuged at 3500 x g for 10 min at 14 °C. The samples were then stored in the dark at -18
114 °C until used for quantitative analysis and antioxidant determination.

115

116 *Ultrasound extraction*

117 Ultrasound-assisted extraction was applied with methanol as a solvent at a sample-to-solvent
118 ratio of 1:100 g/mL of dried sample. The extraction process was conducted in an ultrasonic
119 bath (Soniclean, 220 V, 50 Hz and 250 W, Soniclean Pty Ltd., Thebarton, Australia) with
120 pre-set conditions at temperature of 30 °C, time of 20 min and power of 60W. After
121 completion of the extraction, the extracts were immediately cooled on ice to room
122 temperature, and then centrifuged at 3500 x g for 10 min at 14 °C. The sample supernatant
123 was then collected at storage conditions.

124

125

126 *Experimental design*

127 Response Surface Methodology (RSM) of JMP (Version 11) was applied to design and
128 optimise the conditions for the aqueous extraction of bioactive compounds and antioxidant
129 capacity from lemon pomace. Three parameters including temperature (X_1 : 75-95 °C), time
130 (X_2 : 5-15 min) and sample-to-solvent ratio (X_3 : 1-10 g / 100 mL) were tested. The optimal
131 ranges of these parameters were determined in preliminary experiments. A three-factor and a
132 three-level Box–Behnken design consisting of fifteen experimental runs was employed
133 including three central points replicated in the design of the experimental conditions, since
134 Box–Behnken design is considered as an efficient design for response surface methodology
135 (Ferreira *et al.*, 2007).

136 A second-order polynomial equation was used to express the amount of total phenolic
137 compounds, total flavonoids, proanthocyanidins, and antioxidant capacity. The generalised
138 second-order polynomial model used in the response surface analysis is shown in Eq. (1):

139
$$Y = \beta_0 + \sum_{i=1}^n \beta_i X_i + \sum_{\substack{i=1 \\ i < j}}^{n-1} \sum_{j=i+1}^n \beta_{ij} X_i X_j + \sum_{i=1}^n \beta_{ii} X_i^2 \quad \text{Equation (1)}$$

140 Y is the predicted response, b_0 , b_i , b_{ii} and b_{ij} are the regression coefficients for intercept,
141 linear, quadratic and interaction terms, respectively, and X_i , and X_j are the independent
142 variables (Vuong *et al.*, 2011).

143 For the validation of the model, the optimised conditions of the independent variables were
144 further applied in triplicate, using the same experimental procedure as mentioned previously.

145

146 *Determination of chemical properties*

147 *Total phenolic content (TPC)*: TPC was determined as described by Vuong *et al.* (2013).
148 Briefly, 5 mL of 10% (v/v) Folin-Ciocalteu reagent was added to 1 mL of sample, followed
149 by the addition of 4 mL of 7.5% (w/v) Na_2CO_3 , then mixed well on a vortex for 2 min and
150 incubated in the dark at room temperature for 1 h prior to measurement of solution

151 absorbance ($\lambda = 760$ nm) by UV spectrophotometer (Varian Australia Pty. Ltd., Victoria,
152 Australia). Gallic acid was used as the standard for a calibration curve, with the results
153 expressed as mg of gallic acid equivalents per g of sample dry weight (mg GAE/g dw).

154 *Total flavonoid content (TFC)*: Total flavonoid content was measured as described by
155 Zhishen *et al.* (1999). Briefly 2 mL of H₂O and 0.15 mL of 5% (w/v) NaNO₂ were added to
156 0.5 mL of sample and left at room temperature for 6 min. Then 0.15 mL of 10% (w/v) AlCl₃
157 was added and left at room temperature for 6 min. Subsequently, 2 mL of 4% (w/v) NaOH
158 and 0.7 mL of H₂O were added and the final volume of the mixture left at room temperature
159 for a further 15 min before the absorbance was measured ($\lambda = 510$ nm) using a UV
160 spectrophotometer. Catechin was used as the standard for a calibration curve and the results
161 were expressed as mg of catechin equivalents per g of sample dry weight (mg CE/g dw).

162 *Proanthocyanidins*: Proanthocyanidins were determined according to a method described by
163 Li *et al.* (2006). Vanillin (3 mL, of 4% w/v) was added to 0.5 mL of sample. Subsequently,
164 1.5 mL of concentrated HCl was added to the mixture and left for 15 min at room
165 temperature before the absorbance was measured at 500 nm using a UV spectrophotometer.
166 Catechin was used as the standard for a calibration curve and the results were expressed as
167 milligrams of catechin equivalents per g of sample dry weight (mg CE/g dw).

168

169 *Methods for the determination of antioxidant properties*

170 *DPPH assay*: DPPH (2,2-diphenyl-1-picrylhydrazyl) assay was used for the determination of
171 the antioxidant activity as described by Thaipong *et al.* (2006), with some modifications. A
172 stock solution was prepared by dissolving 24 mg DPPH in 100 mL methanol and then stored
173 at -20 °C until required. The working solution was then prepared fresh by mixing 10 mL
174 stock solution with 45 mL methanol to obtain an absorbance of 1.1 ± 0.02 ($\lambda = 515$ nm).
175 Subsequently, 2.85 mL of working solution was added to 0.15 mL of sample and left under

176 darkness at room temperature for 30 min before measuring the absorbance ($\lambda= 515$ nm) using
177 a UV spectrophotometer. Trolox was used as the standard for a calibration curve and the
178 results were expressed as mg of trolox equivalents per g of sample dry weight (mg TE/g dw).

179 *ABTS assay*: ABTS (2,2'- azino-bis(3-ethylbenzthiazoline-6-sulphonic acid)) assay was used
180 for the determination of the antioxidant activity as described by Thaipong *et al.* (2006) with
181 some modifications. A stock solution was prepared by adding 10 mL of 7.4 mM ABTS
182 solution to 10 mL of 2.6 mM $K_2S_2O_8$ and left at room temperature in the dark for 15 h, and
183 then stored at -20 °C until required. The working solution was freshly prepared by diluting 1
184 mL of stock solution with 60 mL of methanol to obtain an absorbance value of 1.1 ± 0.02 ($\lambda=$
185 734 nm). Subsequently, 2.85 mL of the working solution was then added to 0.15 mL of
186 sample and left in the dark at room temperature for 2 h before its absorbance was recorded
187 ($\lambda= 734$ nm) using a UV spectrophotometer. Trolox was used as a standard and the results
188 were expressed as mg trolox equivalents per g of sample dry weight (mg TE/g dw).

189 *FRAP assay*: FRAP (Ferric reducing antioxidant power) was measured as described by
190 Thaipong *et al.* (2006) with some modifications. A working FRAP solution was prepared by
191 mixing 300 mM acetate buffer, 10 mM Tripyridil-s-triazine (TPTZ) in 40 mM HCl and 20
192 mM $FeCl_3$ in the ratio of 10:1:1 and warmed to 37 °C in a water bath (Ratek Instruments Pty.
193 Ltd., Victoria, Australia). Working FRAP solution (2.85 mL) was added to 0.15 mL of
194 sample and incubated at room temperature in the dark for 30 min before its absorbance was
195 read ($\lambda= 593$ nm) using a UV spectrophotometer. Trolox was used as a standard and the
196 results were expressed as mg trolox equivalents per g of sample dry weight (mg TE/g dw).

197 *CUPRAC assay*: CUPRAC (cupric reducing antioxidant capacity) was determined as
198 described by Apak *et al.* (2004) with some modifications. $CuCl_2$ (1 mL) were mixed with 1
199 mL of neocuproine and 1 mL of NH_4Ac . Subsequently 1.1 mL of sample were added to this
200 mixture. The mixture was incubated at room temperature for 1.5 h before measuring the

201 absorbance ($\lambda = 450$ nm) using a UV spectrophotometer. Trolox was used as the standard for
202 a calibration curve and the results were expressed as mg of trolox equivalents per g of sample
203 dry weight (mg TE/g dw).

204

205 **Statistical analysis**

206 The Pearson correlation test was used to evaluate the correlation between the bioactive
207 compounds and different antioxidant assays. The correlation analysis was performed using
208 SPSS statistical software (version 23), with a p -value < 0.05 considered significant. The
209 predicted and observed values were compared with the least significant difference at $p < 0.05$
210 and expressed as means \pm standard deviations. For the comparison of hot water with
211 methanol extracts, a one-way ANOVA and the Least Significance Difference (LSD) at $p <$
212 0.05 were conducted using SPSS statistical software (version 23). All the experiments were
213 conducted in triplicate.

214

215 **Results and discussion**

216 *Fitting of the models and validation*

217 Fitting of model for the TPC, TF, and proanthocyanidins, was analysed, the results displayed
218 in Table 2 and Figure 1. The RSM application of TPC values showed that the model was
219 significant ($p < 0.003$), did not present lack of fit ($p = 0.066$), the adjusted $R^2 = 0.90$
220 and could explain 97% of all variance in the data.

221 The RSM application of TF values showed that the model was significant ($p <$
222 0.026), presented lack of fit ($p = 0.004$), the adjusted $R^2 = 0.78$ and could explain 92% of all
223 variance in data. For the proanthocyanidins values the RSM application showed that
224 model was not significant ($p < 0.11$), presented lack of fit ($p = 0.001$), the adjusted $R^2 =$
0.58 and could

225 explain 85% of all variance in data. That means that the model is not reliable for the
226 prediction of proanthocyanidin yields.

227 Fitting of model for the antioxidant capacity measured by DPPH, ABTS, FRAP, and
228 CUPRAC was analysed and the results can be seen in Table 2 and Figure 2. The RSM
229 application of DPPH showed that the model was significant ($p < 0.022$), presented lack of fit
230 ($p = 0.002$), the adjusted $R^2 = 0.80$ and could explain 93% of all variance in data. For the
231 ABTS the RSM application showed that the model was significant ($p < 0.002$), did not
232 present lack of fit ($p = 0.065$), the adjusted $R^2 = 0.93$ and could explain 98% of all variance in
233 data. For the FRAP assay, the model was significant ($p < 0.036$), presented lack of fit ($p =$
234 0.001), the adjusted $R^2 = 0.75$ and could explain 91% of all variance in data. Finally, for
235 CUPRAC assay the model was significant ($p < 0.0001$), did not present lack of fit ($p =$
236 0.129), the adjusted $R^2 = 0.98$ and could explain 99% of all variance in data. In general,
237 analysis of results revealed that the mathematical models are reliable for the prediction of
238 bioactive compounds and antioxidant properties and are expressed and fitted in the following
239 equations.

$$240 \quad Y_{TPC} = 5.27333 + 0.077875 \times (X_1-85) + 0.1455 \times (X_2-10) - 0.6222 \times (X_3-5.5) - 0.00035 \times$$
$$241 \quad (X_1 \times X_2 - 10 \times X_1 - 85 \times X_2 + 850) - 0.02944 \times (X_1 \times X_3 - 5.5 \times X_1 - 85 \times X_3 + 467.5) + 0.03055 \times (X_2 \times X_3 -$$
$$242 \quad 5.5 \times X_2 - 10 \times X_3 + 55) + 0.0055333 \times (X_1 - 85)^2 + 0.0636 \times (X_2 - 10)^2 + 0.094485 \times (X_3 - 5.5)^2$$

243 Equation (2)

244

$$245 \quad Y_{TF} = 1.75 + 0.01025 \times (X_1-85) - 0.01375 \times (X_2-10) - 0.24861 \times (X_3-5.5) - 0.0047 \times (X_1 \times X_2 -$$
$$246 \quad 10 \times X_1 - 85 \times X_2 + 850) - 0.0017 \times (X_1 \times X_3 - 5.5 \times X_1 - 85 \times X_3 + 467.5) - 0.0057 \times (X_2 \times X_3 -$$
$$247 \quad 5.5 \times X_2 - 10 \times X_3 + 55) - 0.0031875 \times (X_1 - 85)^2 + 0.00315 \times (X_2 - 10)^2 + 0.03648 \times (X_3 - 5.5)^2 \text{ (Equation 3)}$$

248

249 $Y_{DPPH} = 0.078033 + 0.0007625 \times (X_1-85) - 0.000815 \times (X_2-10) - 0.0088833 \times (X_3-5.5) -$
250 $0.0000335 \times (X_1 \times X_2 - 10 \times X_1 - 85 \times X_2 + 850) - 0.00014 \times (X_1 \times X_3 - 5.5 \times X_1 - 85 \times X_3 + 467.5) +$
251 $0.00068 \times (X_2 \times X_3 - 5.5 \times X_2 - 10 \times X_3 + 55) + 0.000153 \times (X_1-85)^2 - 0.000156 \times (X_2-10)^2 +$
252 $0.00074 \times (X_3-5.5)^2$ (Equation 4)

253

254 $Y_{ABTS} = 0.086367 + 0.0035975 \times (X_1-85) + 0.006585 \times (X_2-10) - 0.0148 \times (X_3-5.5) +$
255 $0.000326 \times (X_1 \times X_2 - 10 \times X_1 - 85 \times X_2 + 850) - 0.0011 \times (X_1 \times X_3 - 5.5 \times X_1 - 85 \times X_3 + 467.5) -$
256 $0.001462 \times (X_2 \times X_3 - 5.5 \times X_2 - 10 \times X_3 + 55) + 0.000192 \times (X_1-85)^2 + 0.001036 \times (X_2-10)^2 +$
257 $0.0022 \times (X_3-5.5)^2$ (Equation 5)

258

259 $Y_{FRAP} = 4.3329 + 0.064045 \times (X_1-85) + 0.0025275 \times (X_2-10) - 0.413808 \times (X_3-5.5) -$
260 $0.0058105 \times (X_1 \times X_2 - 10 \times X_1 - 85 \times X_2 + 850) - 0.019195 \times (X_1 \times X_3 - 5.5 \times X_1 - 85 \times X_3 + 467.5) +$
261 $0.007098 \times (X_2 \times X_3 - 5.5 \times X_2 - 10 \times X_3 + 55) + 0.003956 \times (X_1-85)^2 - 0.034303 \times (X_2-10)^2 +$
262 $0.015504 \times (X_3-5.5)^2$ (Equation 6)

263

264 $Y_{CUPRAC} = 14.50793 + 0.2775875 \times (X_1-85) + 0.1329075 \times (X_2-10) - 2.0336194 \times (X_3-5.5) -$
265 $0.033289 \times (X_1 \times X_2 - 10 \times X_1 - 85 \times X_2 + 850) - 0.0617511 \times (X_1 \times X_3 - 5.5 \times X_1 - 85 \times X_3 + 467.5) -$
266 $0.0647056 \times (X_2 \times X_3 - 5.5 \times X_2 - 10 \times X_3 + 55) + 0.01823845 \times (X_1-85)^2 + 0.1032048 \times (X_2-10)^2 +$
267 $0.1673763372 \times (X_3-5.5)^2$ (Equation 7)

268

269 *Effect of Extraction parameters on Total Phenolic Compounds (TPC), Total Flavonoids (TF),*
270 *and Proanthocyanidins*

271 The effect of the extraction variables on TPC, TF, and proanthocyanidins can be seen in
272 Table 3. Extraction temperature, and time had a positive significant linear effect on TPC,
273 while sample-to-solvent ratio had a negative significant linear effect on the TPC, TF, and

274 proanthocyanidins. Ratio had a positive significant quadratic effect on TPC and TF, while
275 extraction time had a positive significant quadratic effect only on TPC. A significant
276 interaction effect between extraction temperature and ratio on TPC was observed. The impact
277 of temperature (75–95 °C), time (5–15 min), and sample-to-solvent ratio (1–10 g / 100 mL)
278 on TPC can be seen on Figure 3. The extraction yields of TPC, TF, and proanthocyanidins
279 varied from 3.77 to 12.41 mg GAE/g dw, 0.81 to 4.07 mg CE/g dw, and 0.57 to 1.86 mg
280 CE/g dw, respectively. Overall, an increase in sample-to-solvent ratio tends to decrease the
281 extraction yields of TPC, TF, and proanthocyanidins, while an increase of extraction
282 temperature and time tends to increase the extraction yields of TPC. These results are in
283 agreement with Xu *et al.* (2008) who have reported that hot water led to increased extraction
284 yields of phenolic compounds in two citrus varieties and Hayat *et al.* (2009) who mentioned
285 that the extraction yield of phenolic acids in citrus mandarin increased when the liquid-to-
286 solid ratio increased. The high temperature may affect positively the extraction yields i) by
287 enhancing the solubility of phenolic compounds and the mass transfer rate (Dai and Mumper,
288 2010), as well as ii) by weakening the plant tissues (Al-Farsi and Chang, 2008), while an
289 decrease sample-to-solvent may promote the extraction of bioactive compounds from plant
290 materials, since a larger solvent volume can generally dissolve the bioactive ingredients
291 contained in the sample more effectively (Zhang *et al.*, 2011).

292

293 *Effect of Extraction parameters on antioxidant capacity measured by DPPH, ABTS,*
294 *FRAP, and CUPRAC*

295 The antioxidant activity of lemon pomace extracts was determined using four antioxidant
296 assays including DPPH, ABTS, FRAP and CUPRAC, since each antioxidant assay has its
297 own advantages and limitations (Vuong *et al.*, 2015).

298 The effect of extraction variables on antioxidant capacity of lemon pomace extracts can be
299 seen in Table 4. Sample-to-solvent ratio had a significant negative linear effect on the
300 antioxidants measured by all assays ($p < 0.001$). These results are in accord with
301 Candrawinata *et al.* (2015) who mentioned that an increase in apple pomace-to-water ratio led
302 to a decrease in the antioxidant activity of the extracts. Extraction temperature had a linear
303 effect on the antioxidants measured by ABTS and CUPRAC (positive effect, $p < 0.01$), while
304 time had a positive linear effect only on the antioxidants measured by ABTS at a level of
305 significance of $p < 0.01$. Both extraction temperature and time had no effect on the
306 antioxidants measured by DPPH and FRAP which is in accord with Xu *et al.* (2008) who
307 mentioned that extraction temperature and time had very little impact on the antioxidant
308 capacity of hot water citrus peel extracts. A positive quadratic effect of the extraction time
309 and ratio on the antioxidants measured by CUPRAC ($p < 0.01$) and ABTS ($p < 0.05$ and $p <$
310 0.01 , respectively) was observed. The interaction between temperature and ratio had a
311 negative effect on both ABTS and CUPRAC values ($p < 0.01$ and $p < 0.05$, respectively),
312 while the interaction between time and ratio had a negative effect only on the antioxidants
313 measured by ABTS assay at a level of significance of $p < 0.05$. The antioxidant activity
314 varied from 0.1697 to 1.3806 mg TE/g dw (DPPH), 0.3014 to 2.0067 mg TE/g dw (ABTS),
315 2.1243 to 9.2256 mg TE/g dw (FRAP), and 10.1438 to 34.8561 mg TE/g dw (CUPRAC).
316 Overall, an increase in sample-to-solvent ratio tends to decrease the antioxidant activity of the
317 extracts, which is consistent with the mass transfer principle where the driving force for mass
318 transfer is considered to be the concentration gradient between the solid and the solvent (Al-
319 Farsi and Chang, 2008; Tan *et al.*, 2011).

320

321 *Correlation between TPC, TF, proanthocyanidins and antioxidant capacity.*

322 The contribution of TPC, TF, and proanthocyanidins to the total antioxidant activity can be
323 evaluated by the correlation between them and the antioxidant assays were used
324 (Candrawinata *et al.*, 2015). The r values between TPC and DPPH, ABTS, FRAP, and
325 CUPRAC were 0.75, 0.86, 0.70, and 0.92 ($p<0.01$), respectively, revealing that TPC was a
326 major contributor to the antioxidant properties of the lemon pomace extracts. Similarly, the r
327 values between TF and DPPH, ABTS, FRAP, and CUPRAC were 0.76, 0.66, 0.67 and 0.86
328 ($p<0.01$), respectively, indicating that TF contribute to the antioxidant activity of lemon
329 pomace, as well. The r values between proanthocyanidins and DPPH, ABTS, FRAP, and
330 CUPRAC were 0.75, 0.52, 0.51 and 0.61 ($p<0.01$), respectively, indicating that
331 proanthocyanidins have a lower contribution to the antioxidant activity of lemon pomace
332 compared to the TPC and TF (Table 5). These results are supported by previous studies
333 which indicated that TPC had close correlation with antioxidant character and was the major
334 contributor to the antioxidant properties of citrus extracts, because of their potential electron
335 donor capacity, due to the usual presence of multiple hydroxyl groups (Lagha-Benamrouche
336 and Madani, 2013; Shofinita *et al.*, 2015). In contrast, Ghasemi *et al.* (2009) reported no
337 correlation between phenolic compounds or flavonoids and antioxidant activity of citrus
338 peels. This difference could be attributed to the different extraction method and solvent used
339 by this study.

340

341 *Optimisation of aqueous extraction conditions for bioactive compounds and antioxidant*
342 *properties from lemon pomace.*

343 Based on the RSM predictive models and expected values, the optimal conditions for the total
344 phenolic compounds, flavonoids, proanthocyanidins, and all four different antioxidant assays
345 were selected at temperature = 95 °C, time = 15 min, and sample-to-solvent ratio = 1:100 g /
346 mL. To validate the model, three individual experiments were performed under the optimal

347 conditions. The results presented in Table 6, show no significant difference between the
348 predicted and observed values, therefore, these conditions were recommended for optimal
349 extraction of lemon pomace for analysis of bioactive compounds and antioxidant properties.

350

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352

353 *Comparison with methanol extracts obtained by ultrasound assisted extraction*

354 The TPC, TF, proanthocyanidins, DPPH, ABTS, and CUPRAC values obtained by the
355 optimal conditions from the hot water extraction were compared with methanol extract
356 values. The same lemon pomace was used for both hot water and methanol extractions.
357 Analysis of variance showed that there was no significant difference between the values
358 obtained by hot water and methanol for the TPC, TF, and the antioxidant capacity determined
359 by DPPH and ABTS at $p < 0.05$. However, methanol extracts contained 48.27% more
360 proanthocyanidins than water extracts and CUPRAC values were 39.82% greater for the
361 methanol compared to the hot water extracts (Table 7). Dahmoune *et al.* (2013) reported that
362 the optimal microwave extraction conditions using ethanol as a solvent in lemon pomace
363 resulted in TPC yields of 15.78 ± 0.80 mg GAE/g which are close to the yields obtained at
364 the optimal conditions by hot water in this experiment. The efficiency of hot water could be
365 attributed to the high temperature enhancing the solubility of bioactive compounds leading in
366 higher extraction yields (Davidov-Pardo *et al.*, 2011). These results are in agreement with Xu
367 *et al.* (2008) who supported that hot water extracts from citrus peels had the same antioxidant
368 capacity with methanol extracts.

369

370 *Conclusion*

371 Box-Behnken experimental design was effective in evaluating the effect of extraction
372 temperature, time, and sample-to-solvent ratio on the total phenolic compounds, flavonoids
373 and antioxidant capacity measured by DPPH, ABTS, FRAP, and CUPRAC. Sample-to-
374 solvent ratio was the factor that influenced negatively all the dependent variables, revealing
375 that when the sample-to-solvent ratio increased the dependent variables decreased. Lemon
376 pomace is a good source of TPC and TF since high correlation was observed between them
377 and the antioxidant capacity assays. The optimum conditions for increasing the yield of total
378 phenolic content, total flavonoid compounds and antioxidant capacity were obtained at 95 °C
379 temperature, 15 min extraction time, and 1 g / 100 ml sample-to-water. Hot water extracts at
380 the optimal conditions had the same content of TPC and TF as methanol extracts obtained by
381 ultrasound extraction. Overall, hot water could be an effective solvent for the recovery of
382 TPC, TF from lemon pomace.

383

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388

389 **Conflict of interest statement**

390 The authors declare no conflict of interest.

391

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502 **Tables and Figures**

503 **Table 1** Box-Behnken design and the dependent responses.

504 **Table 2.** Analysis of variance for the determination of model fitting.

505 **Table 3.** Analysis of variance for the experimental results of total phenolic compounds
506 (TPC), total flavonoids (TF), and proanthocyanidins.

507 **Table 4.** Analysis of variance for the experimental results of antioxidant activity measured by
508 DPPH, ABTS, FRAP, and CUPRAC.

509 **Table 5.** Correlation between bioactive compounds and antioxidant properties of lemon
510 peels.

511 **Table 6.** Validation of the predicted values for TPC, flavonoids, proanthocyanidins, and
512 antioxidant capacity.

513 **Table 7.** Comparison of hot water (water bath) with methanol extracts (ultrasound
514 extraction).

515 **Fig. 1** Correlation between the predicted and experimental values for TPC, flavonoids, and
516 proanthocyanidins.

517 **Fig. 2** Correlation between the predicted and experimental values for DPPH, ABTS, FRAP,
518 and CUPRAC.

519 **Fig. 3** Impact of temperature (75–95 °C), time (5–15 min), and sample-to-solvent ratio (1–10
520 g / 100 mL) on TPC (mg GAE/g dw).

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